



## CO<sub>2</sub> Reduction and Upgrading for e-Fuels Consortium

U.S. DEPARTMENT OF ENERGY

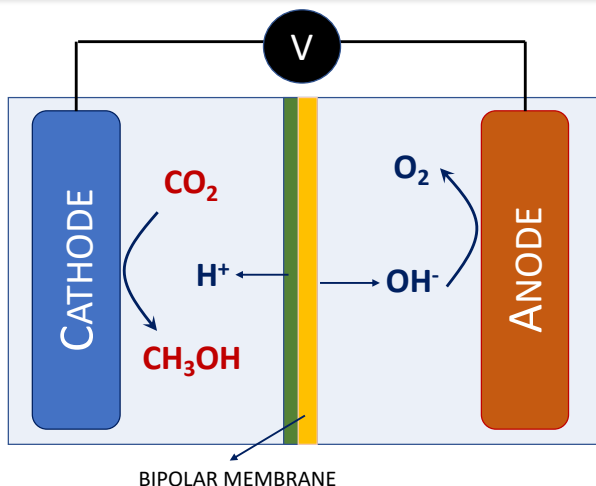
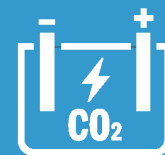
# Electrode and Membrane Materials for CO<sub>2</sub> Electrolyzers: A Molecular Approach

WBS: 2.3.4.304/2.3.4.305

Apr 6 2023

Ksenia Glusac, ANL

# Project Overview: Summary



Electrochemical CO<sub>2</sub> to CH<sub>3</sub>OH conversion:



- Catalysts for selective CO<sub>2</sub> reduction to CH<sub>3</sub>OH
- Bipolar membranes for desired pH and prevention of CH<sub>3</sub>OH crossover.
- Molecular approach: chemically tunable.

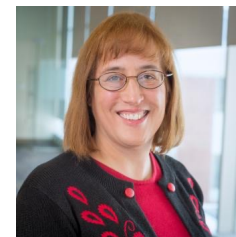
Funding:  
DOE/EERE/Bioenergy Technologies  
Office

Performance Dates:  
Jan 1, 2022 – Sep 30, 2024

TRL: 2-4

## Participants

Glusac/ANL&UIC



Myers/ANL

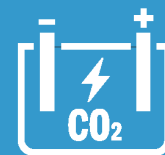
Smith/NREL&CU



Zapol/ANL

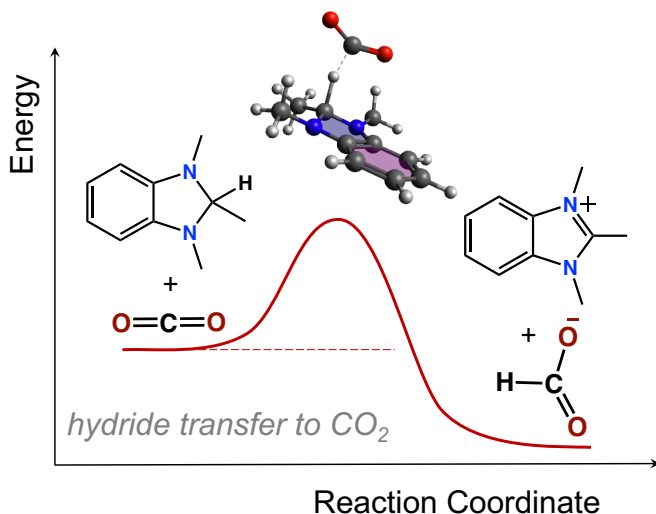


# Project Overview: Glusac Group Expertise



## Molecular bioinspired electrocatalysis/photocatalysis

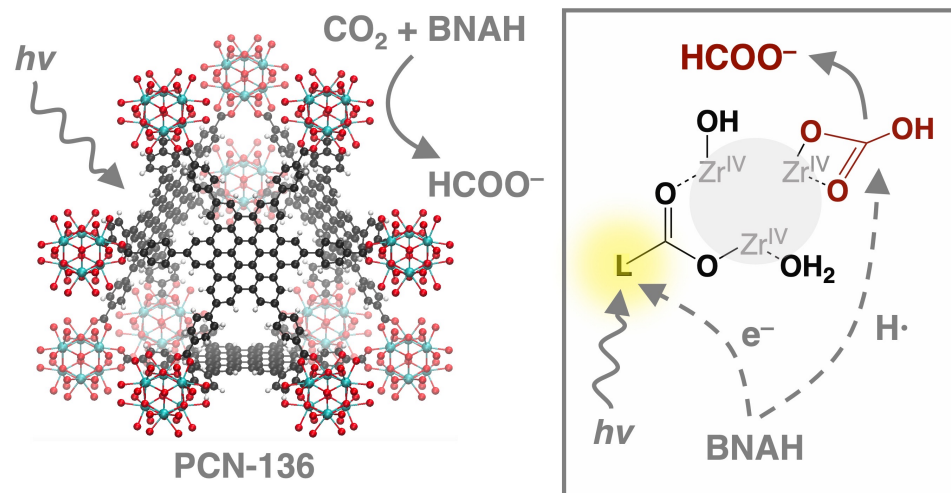
### NADH analogs: CO<sub>2</sub>-to-formate



Accs Chem Res 2022  
J Am Chem Soc 2019  
J Am Chem Soc 2018



### Photoreactive CO<sub>2</sub> capture



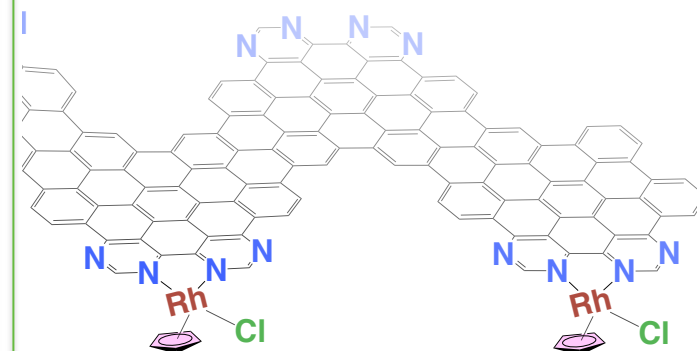
ChemRxiv 2022; ChemRxiv 2023



U.S. DEPARTMENT OF  
**ENERGY**

Office of  
Science

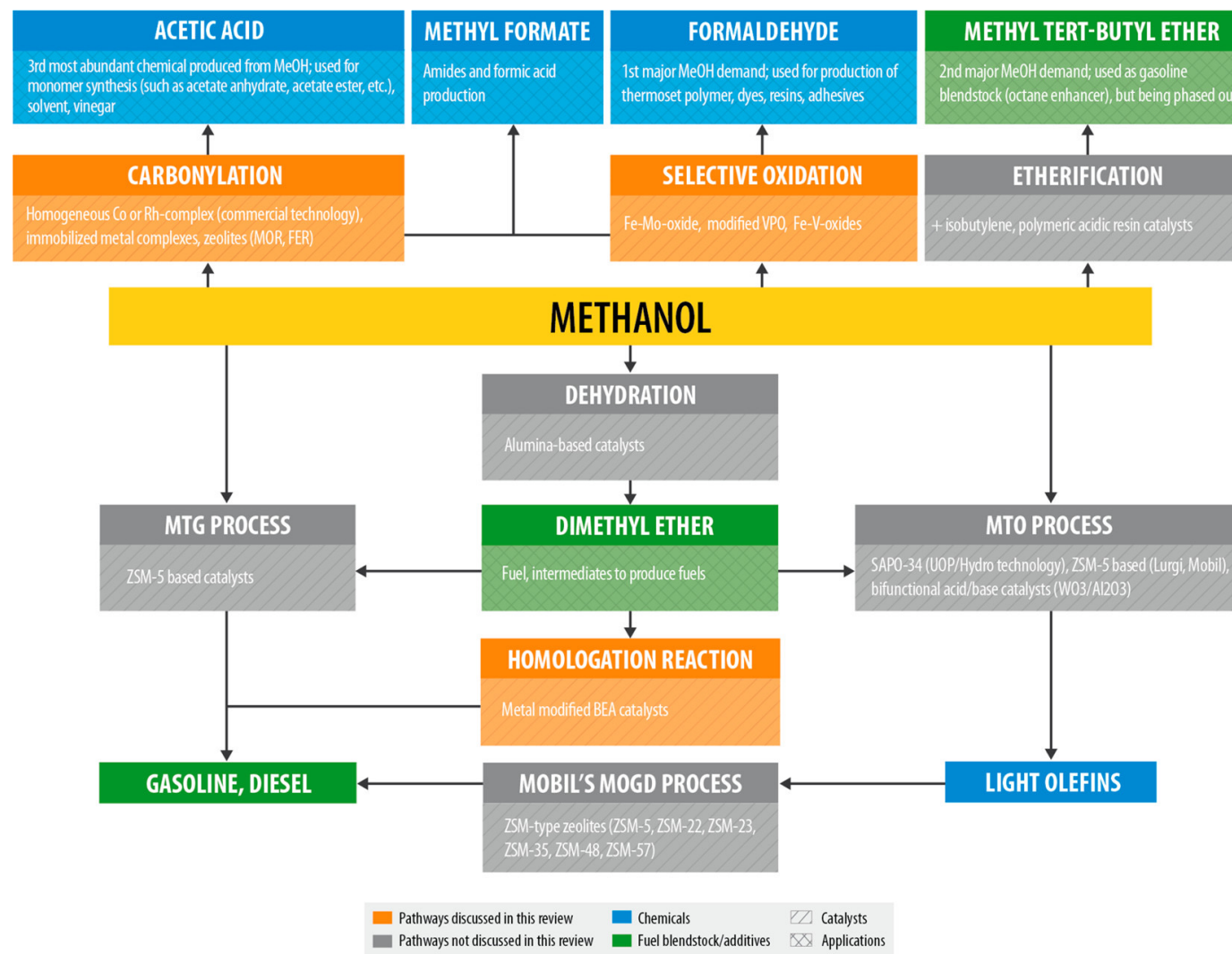
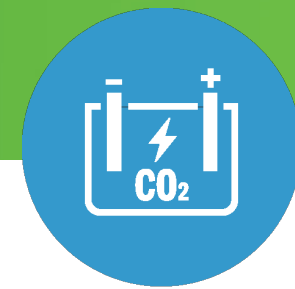
### Molecule/Electrode Hybrid Catalysts



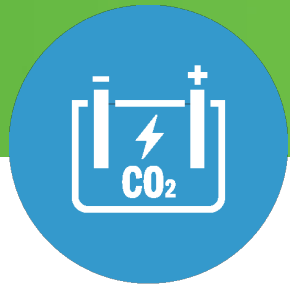
Nat Commun 2021  
ACS Appl Electron  
Mater 2021



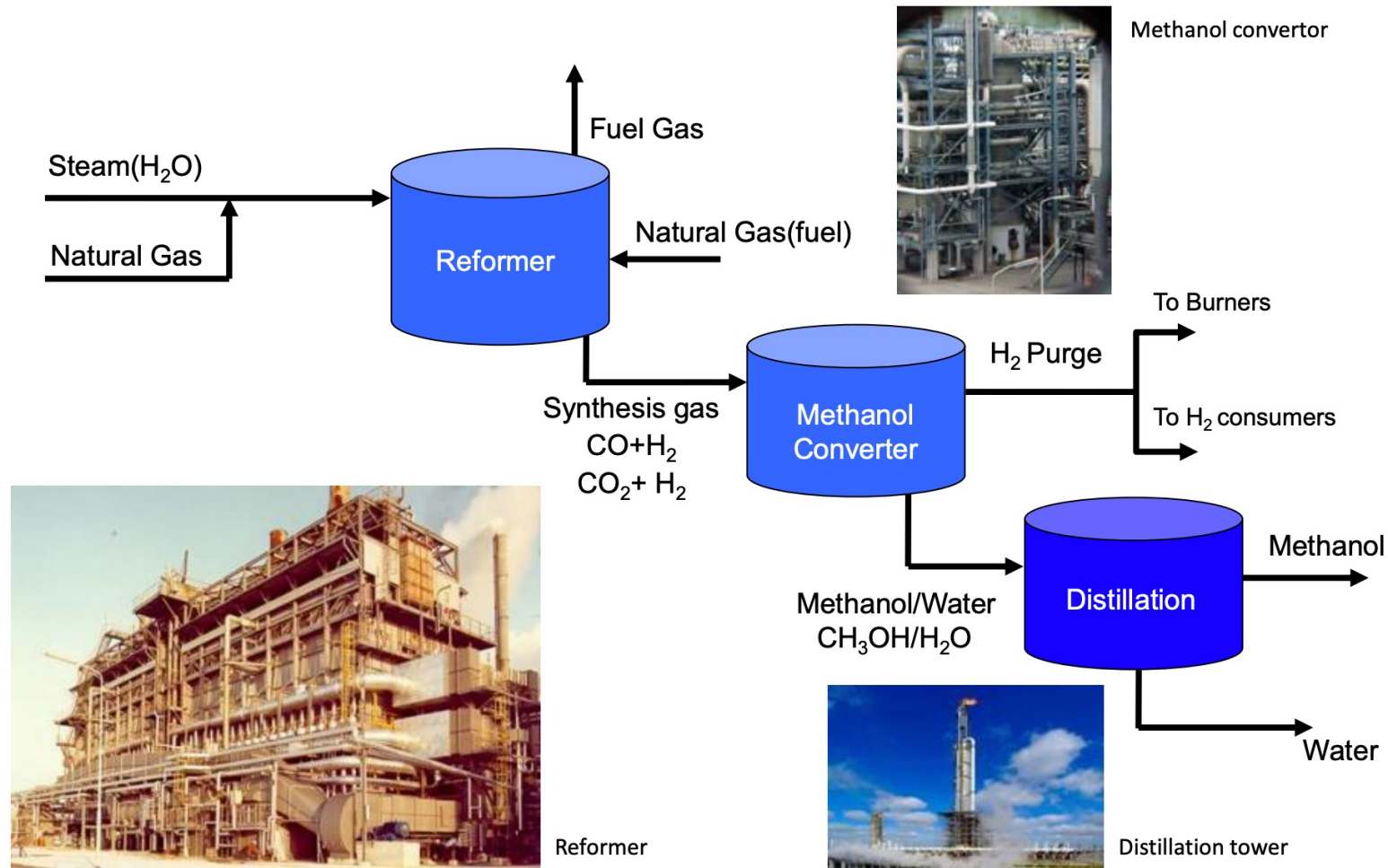
# Project Overview: Methanol as fuel and chemical



# Project Overview: Thermal vs e-Methanol



## Thermal Methanol:

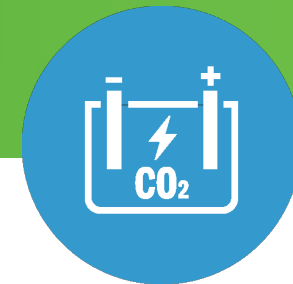


**Non-renewable**  
**2<sup>nd</sup> law of TD**  
**No  $\text{CO}_2$  removal**

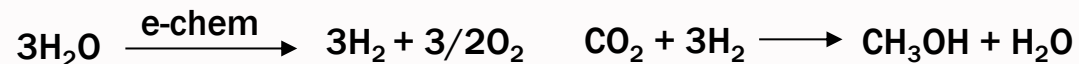




# Project Overview: Thermal vs e-Methanol



**e-METHANOL: Existing plants use a 2-step process**



## E-METHANOL PROJECTS IN THE WORLD:



Company: **Henan/CRI, China**  
Capacity: **110 Kt/y**  
CO<sub>2</sub> source: capture  
Year: **2022**

Company: **DICP, China**  
Capacity: **1 Kt/y**  
CO<sub>2</sub> source: N/A  
Year: **2020**

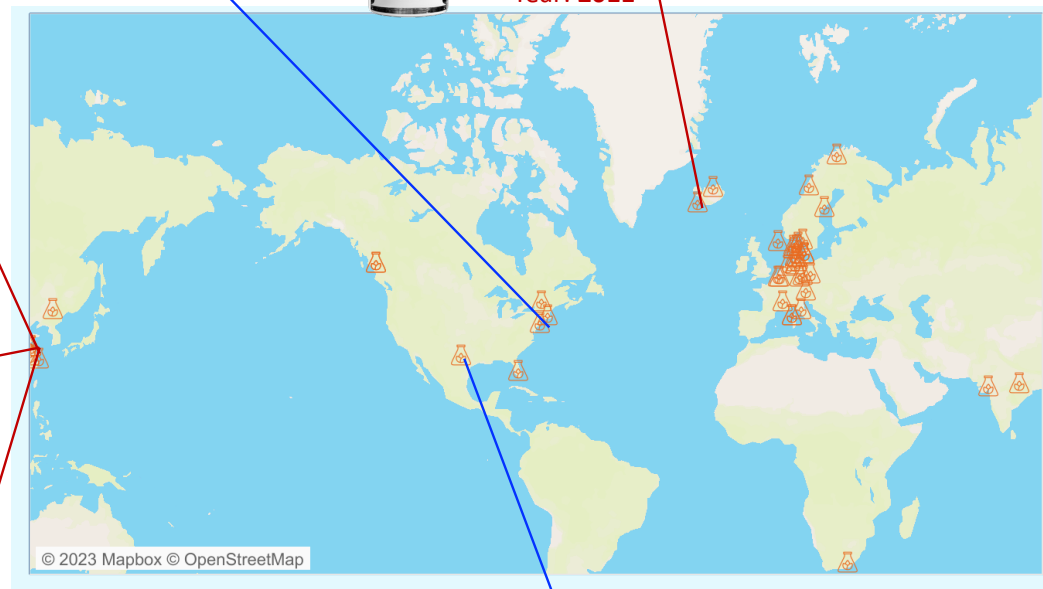
Company: **Blue Chemical, China**  
Capacity: **5 Kt/y**  
CO<sub>2</sub> source: N/A  
Year: **2020**

Company: **Siemens, Porsche, HIF, Chile**  
Capacity: **0.6 Kt/y**  
CO<sub>2</sub> source: DAC  
Year: **2022**

Company: **Air Company, USA**  
Capacity: **0.4 Kt/y**  
CO<sub>2</sub> source: **biogenic**  
Year: **2020**



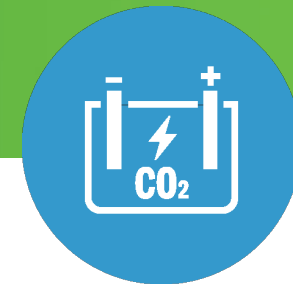
Company: **CRI, Iceland**  
Capacity: **4 Kt/y**  
CO<sub>2</sub> source: **geothermal**  
Year: **2011**



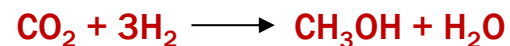
Company: **Celanese, USA**  
Capacity: **80 Kt/y**  
CO<sub>2</sub> source: **recycled**  
Year: **2022**



# Project Overview: e-Methanol number of steps



## Existing plants: 2-step e-Methanol



E-chem is easy

Overall setup is more complicated

More energy used

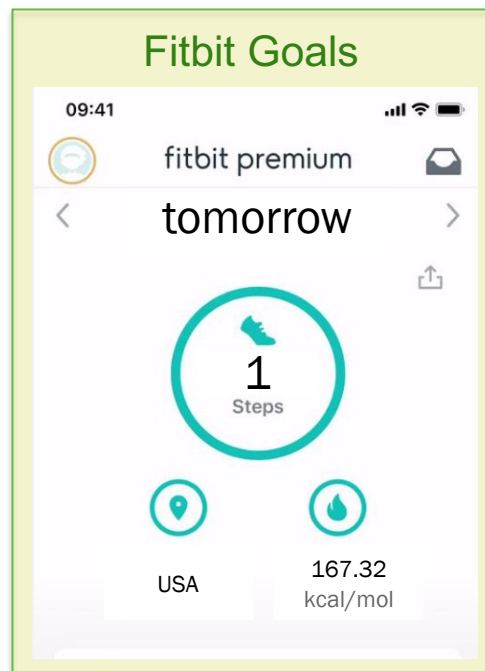
## Our approach: 1-step e-Methanol



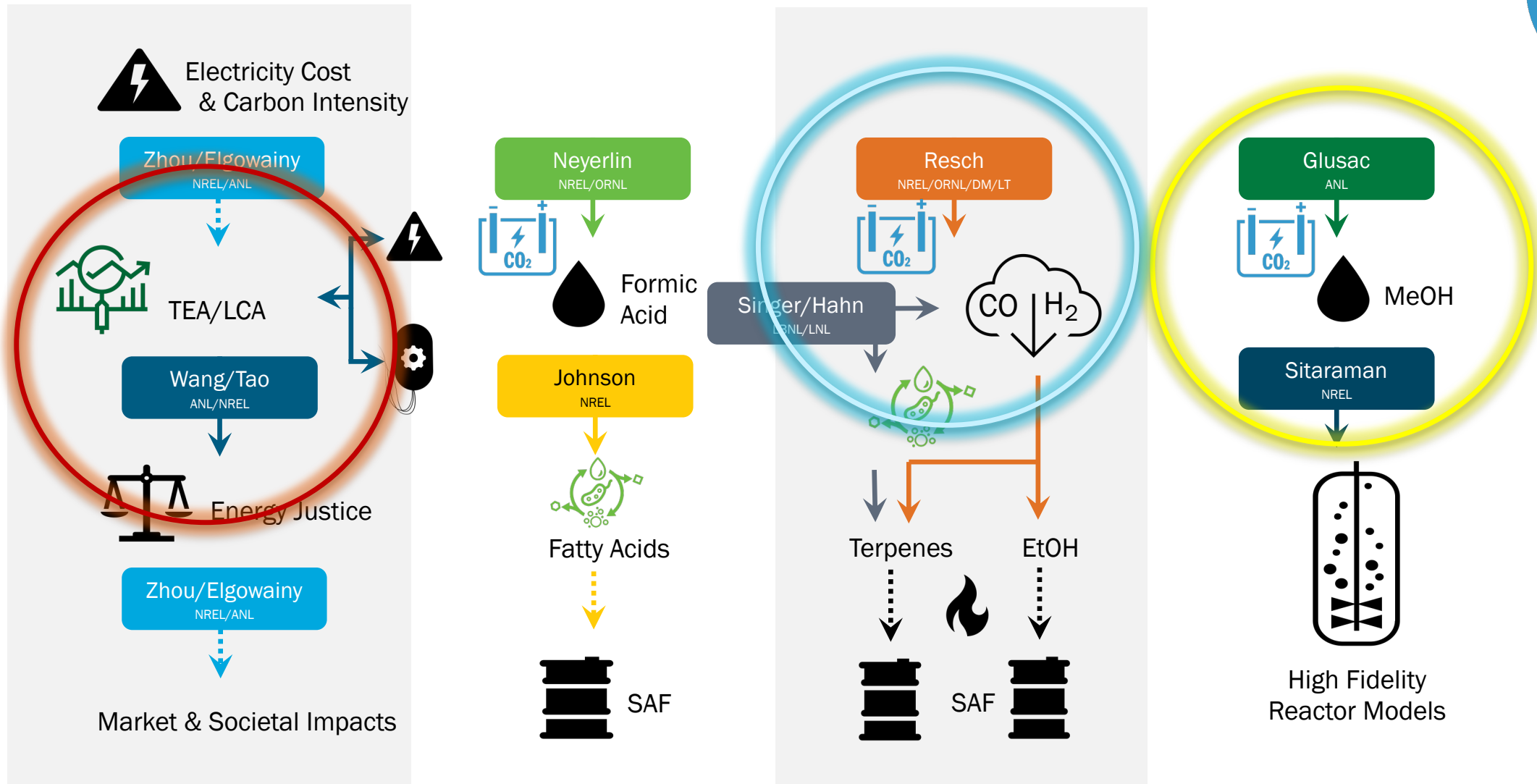
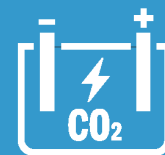
Simpler, all in one step

Less energy used

E-chem more challenging



# Project Overview: Connection with Consortium





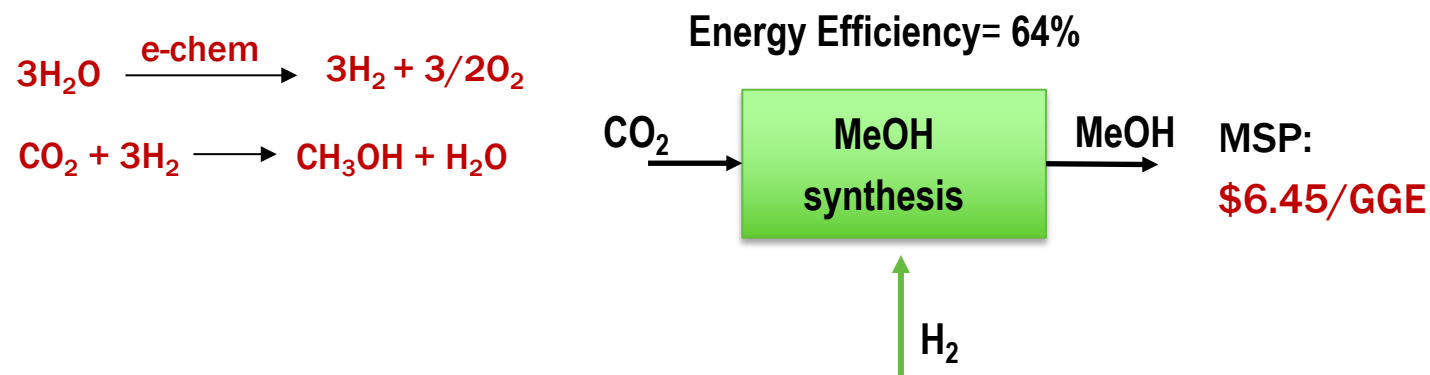
# Project Overview: Connection with Consortium



Ling Tao  
(NREL)

TEA Analysis of two-step and one-step e-methanol production:

## Existing plants: 2-step e-Methanol



Electricity cost: **\$0.068/kWh**;  $\text{H}_2$  cost: **\$4.5/kg**

## Our approach: 1-step e-Methanol



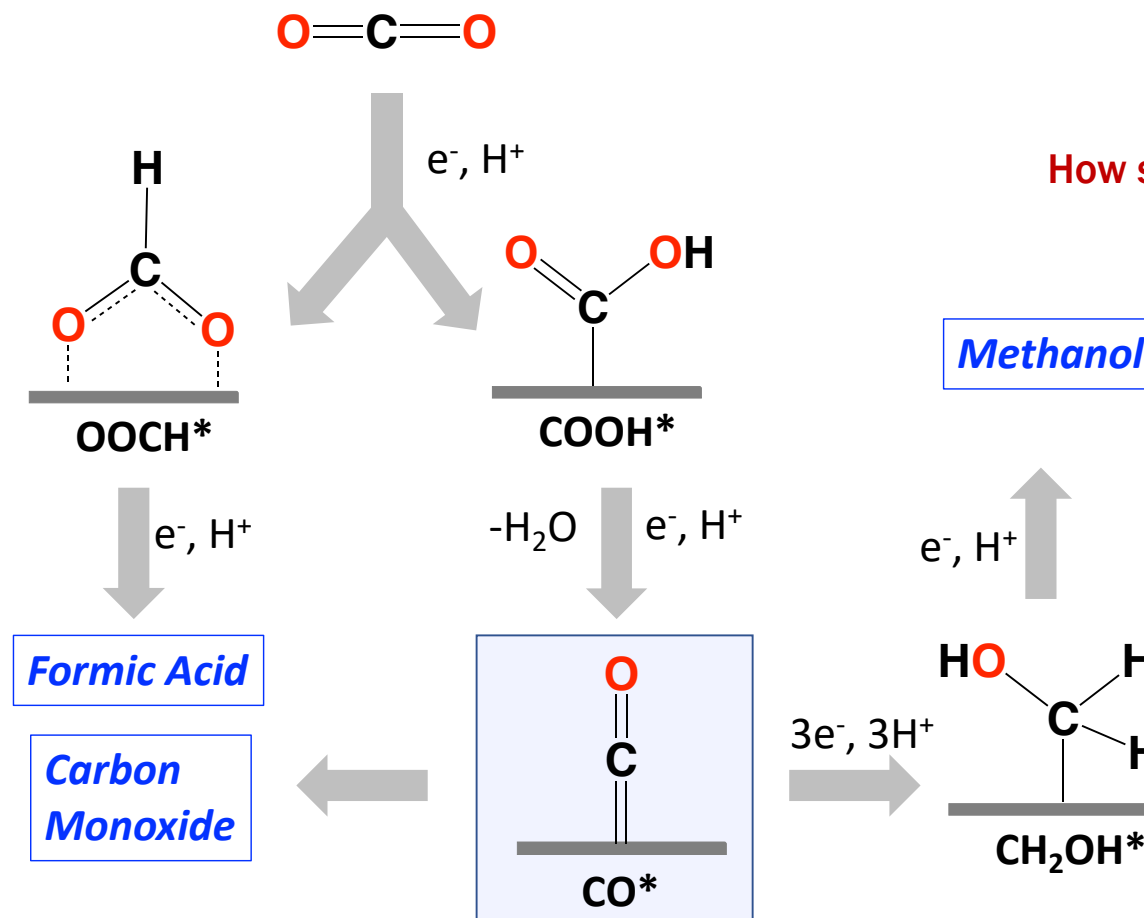
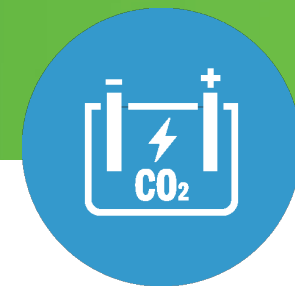
Work in progress.

Goal: to identify what electrolyzer performance we need to achieve to make a single-step methanol generation economically competitive with a two-step process.



Jenny Huang  
(NREL)

# Approach: Theoretical Background



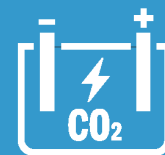
How strongly should CO bind to the electrode?

Too weakly: CO formation  
Too strongly: electrode poisoning  
Just right: CH<sub>3</sub>OH formation

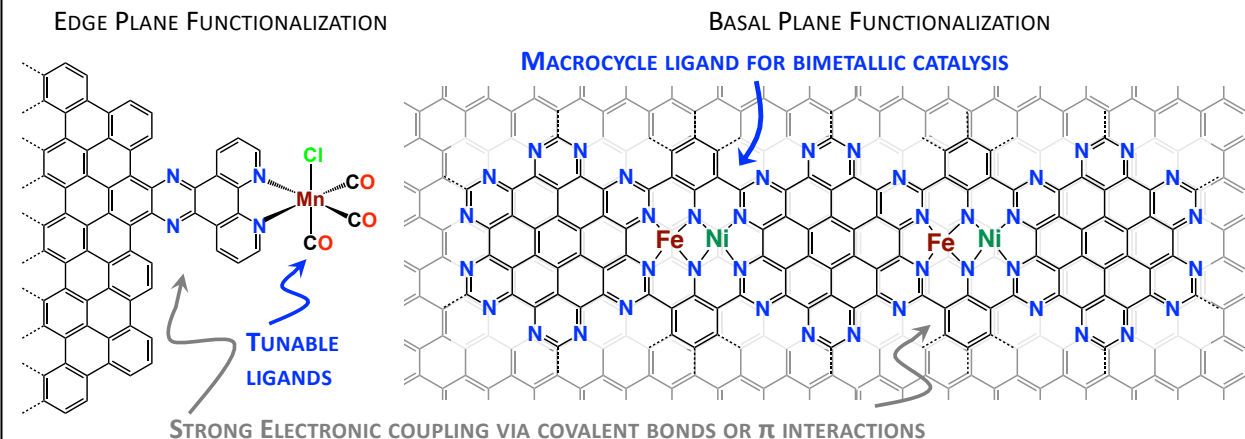
Progress and Perspectives of Electrochemical CO<sub>2</sub> Reduction on Copper in Aqueous Electrolyte  
*Chemical Reviews* **2019** 119 (12), 7610-7672; DOI: 10.1021/acs.chemrev.8b00705



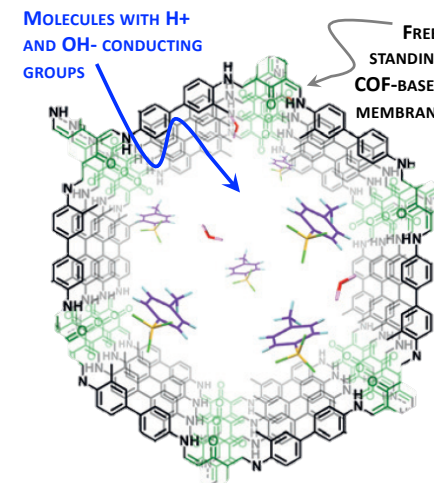
# Approach: Tasks



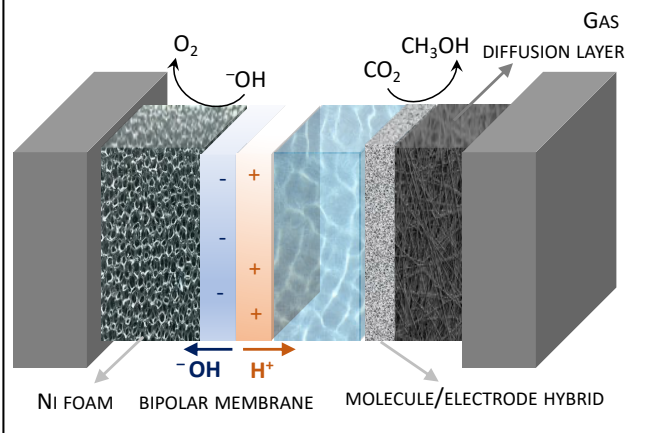
## A. MOLECULE/ELECTRODE HYBRID CO<sub>2</sub>RR CATALYST



## B. COF-BASED MEMBRANES



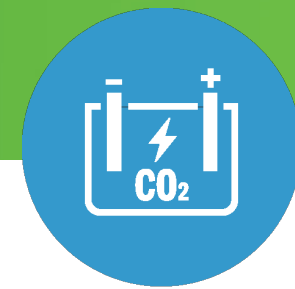
## C. CO<sub>2</sub>RR ELECTROLYZER



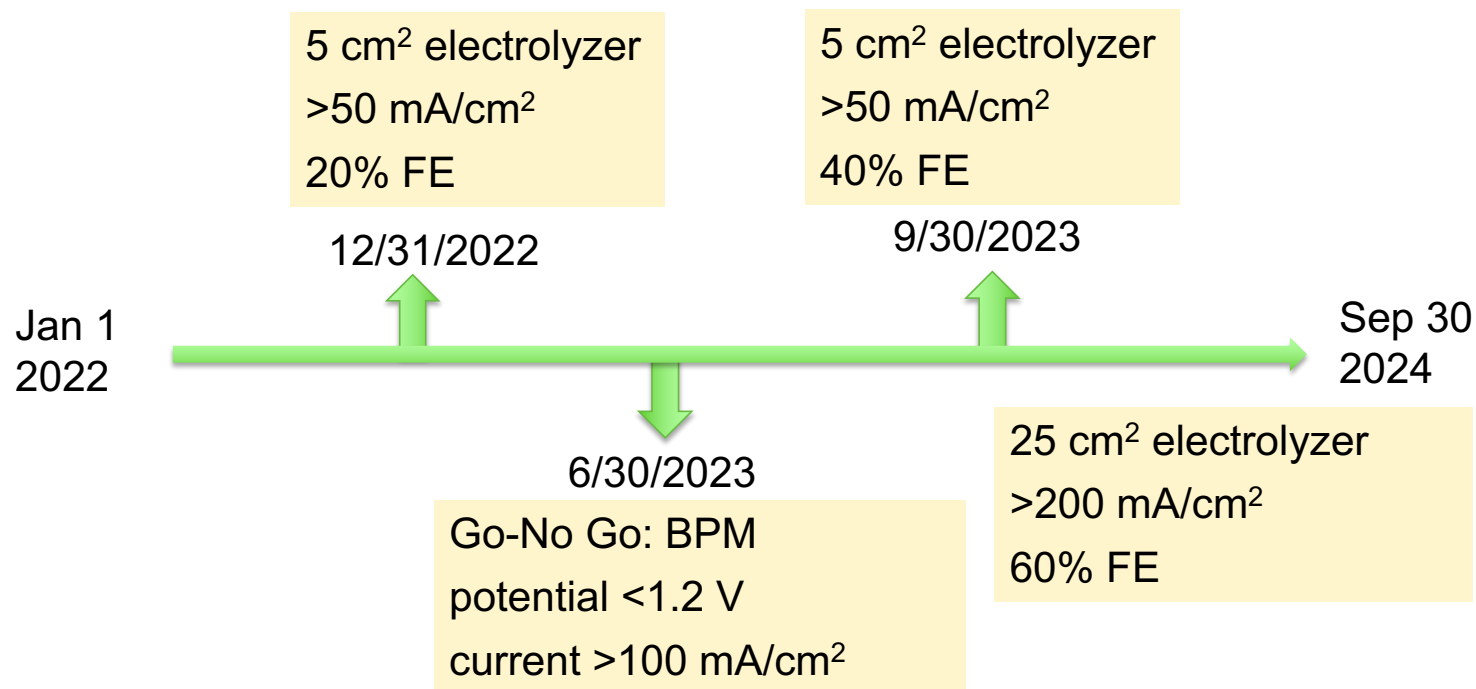
- **Task 1.** Carbon electrode functionalization with molecular catalysts (Glusac, Myers, Zapol).
- **Task 2.** COF-based membranes for H<sup>+</sup>/OH<sup>-</sup> conduction and prevention of methanol crossover (Glusac, Smith).
- **Task 3.** CO<sub>2</sub>R electrolyzer coupled with anodic water oxidation (Smith).



# Approach: Tasks



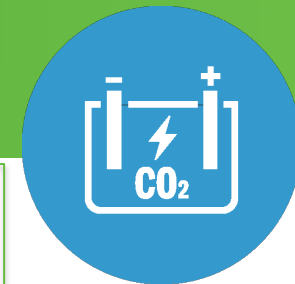
## Project Milestones:



Milestone Name/Description	End Date	Type
Task 2: COF-based bipolar membrane work: demonstration of the reverse-bias water dissociation transmembrane potential of <1.2 V at current densities >100 mA/cm <sup>2</sup> (ANL/NREL)	12/31/2022	Quarterly Progress Measure
Task 1: Finish the computational screening of bimetallic catalysts. Calculate energy landscape for CO <sub>2</sub> reduction to C1 products (CH <sub>3</sub> OH, CO, HCOOH) for at least 15 homonuclear and heterodinuclear complexes (ANL).	03/31/2023	Quarterly Progress Measure
Task 1: Successful synthesis and characterization of at least 3 new electrode materials. The Co-based transition metal complexes will be made and attached to the carbon electrodes. Each electrode material will be made on the 100 mg scale.	06/30/2023	Quarterly Progress Measure
Task 3: Finish CO <sub>2</sub> R electrolyzer testing using Co-complex/CNT cathode catalyst, a commercial BPM, and a NiFe-based anode catalyst. Target performance: 5 cm <sup>2</sup> electrolyzer operating at up to 50 mA/cm <sup>2</sup> with >40% methanol Faradaic efficiency (ANL and NREL).	9/30/2023	Annual SMART Milestone
COF-based BPM work: reverse-bias water dissociation transmembrane potential <1.2 V at current densities >100 mA/cm <sup>2</sup> . No Go pivot: stop exploring bipolar membranes and focus on cathode materials.	6/30/2023	Go/No Go
25 cm <sup>2</sup> electrolyzer operating at >200 mA/cm <sup>2</sup> for at least 100 hrs while maintaining methanol selectivity of 60% Faradaic efficiency.	12/31/2024	End of Project Milestone



# Approach: Experimental Details

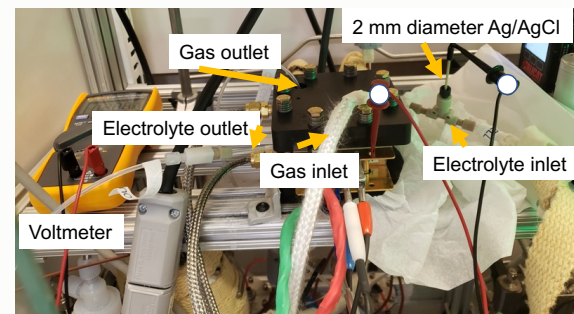


## 3-ELECTRODE MEASUREMENTS



Only the cathodic process monitored.  
Electrode area:  $0.5 \text{ cm}^2$   
Controlled potential electrolysis  
Product detection measured at each potential.  
Faradaic efficiency determined from the charge that passes through.

## CO<sub>2</sub> ELECTROLYZER

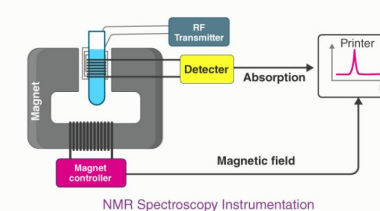


- Both cathodic and anodic ( $\text{O}_2$  evolution) processes monitored.
- Electrode area: several  $\text{cm}^2$
- Controlled current electrolysis

## Product detection:



GC for volatile  
products:  $\text{CO}$  and  $\text{H}_2$



NMR for liquid  
products:  $\text{CH}_3\text{OH}$

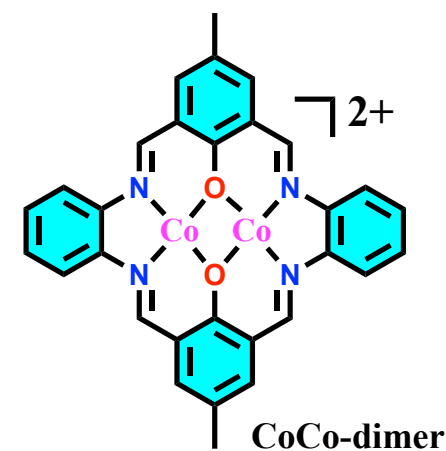
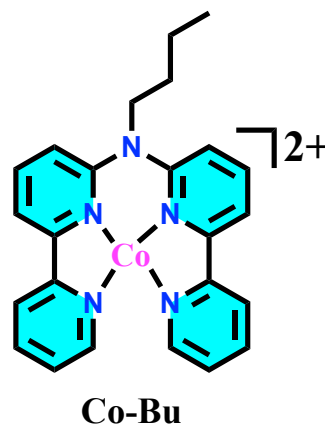
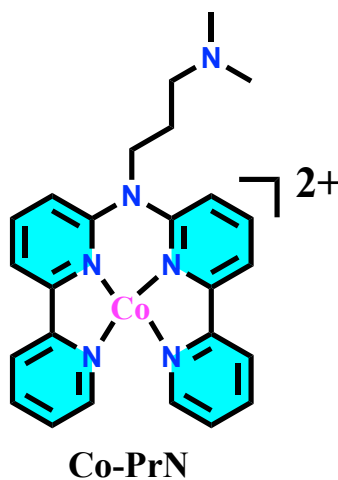
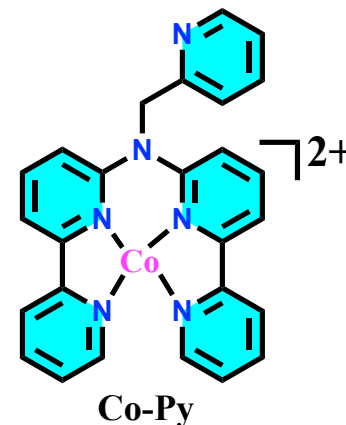
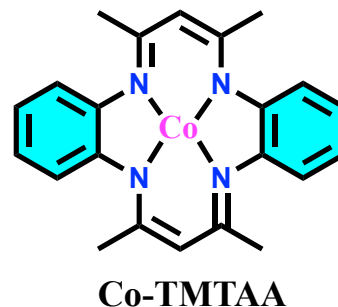
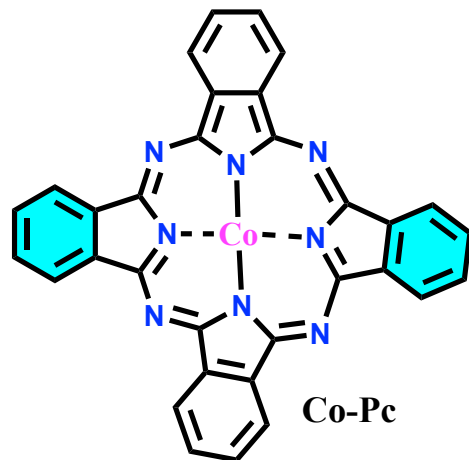


# Progress and Outcomes: Task 1



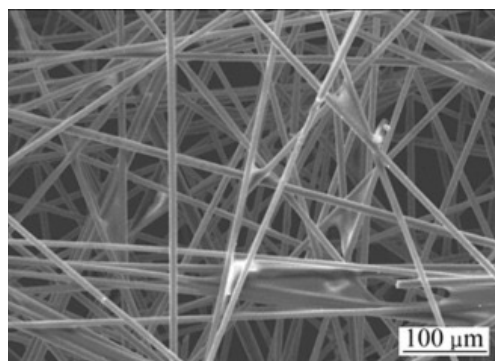
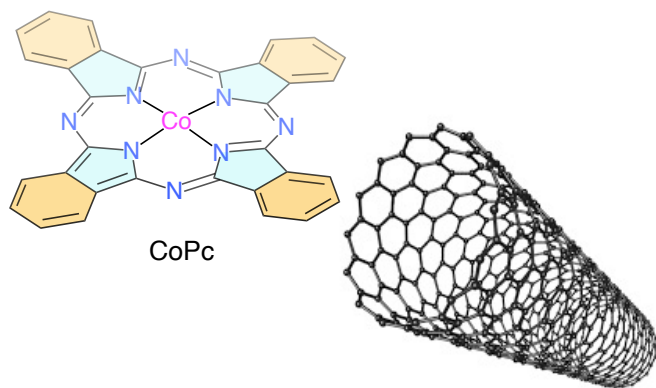
Sreenivasulu  
Chinnabattigalla  
(Glusac)

New Co-  
macrocycles  
synthesized:





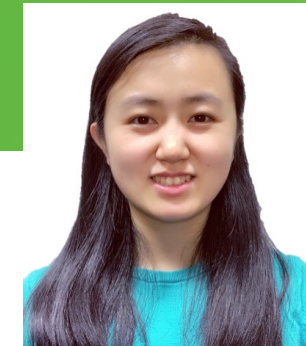
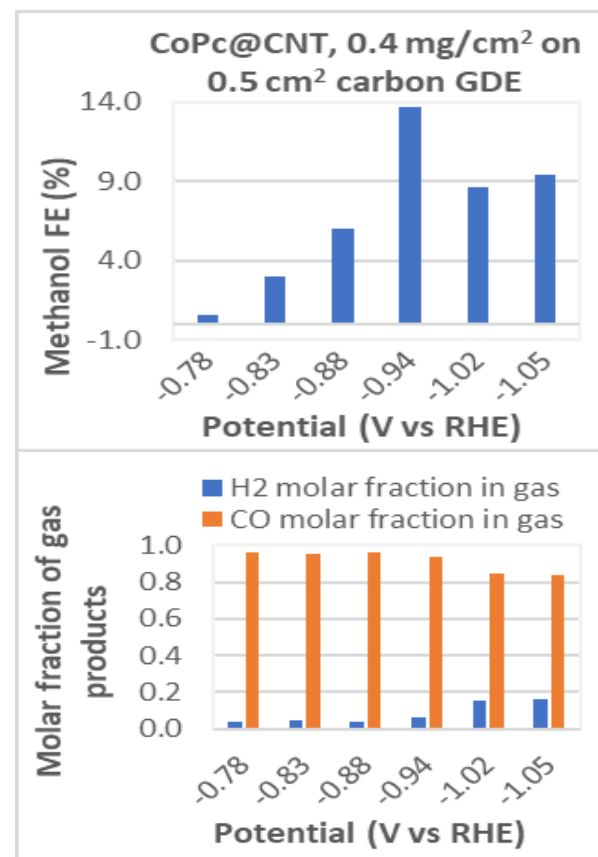
# Progress and Outcomes: Task 1



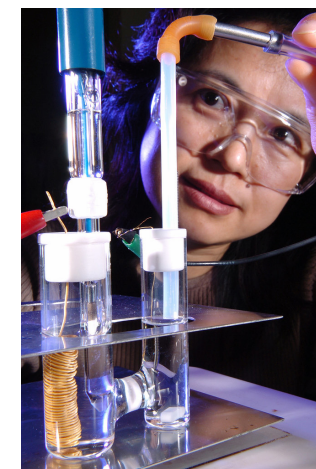
CF

Molecular catalyst immobilized on the carbon electrode:  $\text{CH}_3\text{OH}$  formation observed.

3-electrode test:  
**14%  $\text{CH}_3\text{OH}$  FE at -0.94 V vs RHE**  
(44% is the literature report)



Alice Zheng  
(Glusac)

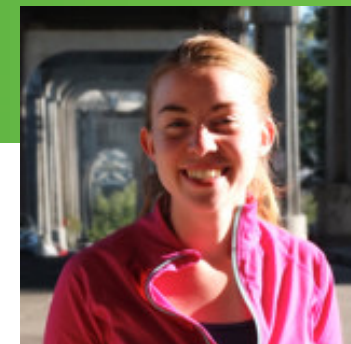
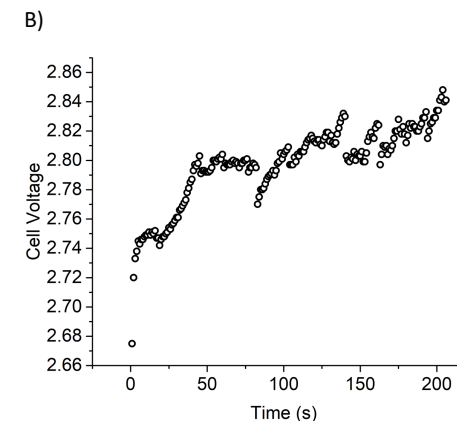
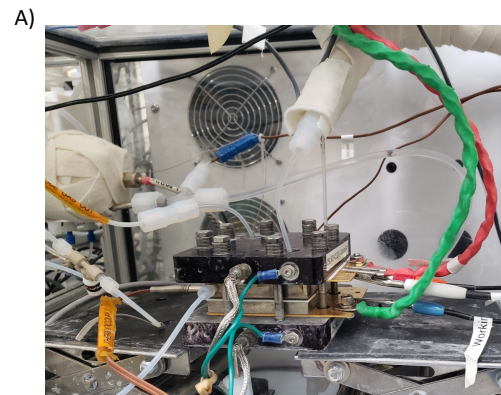
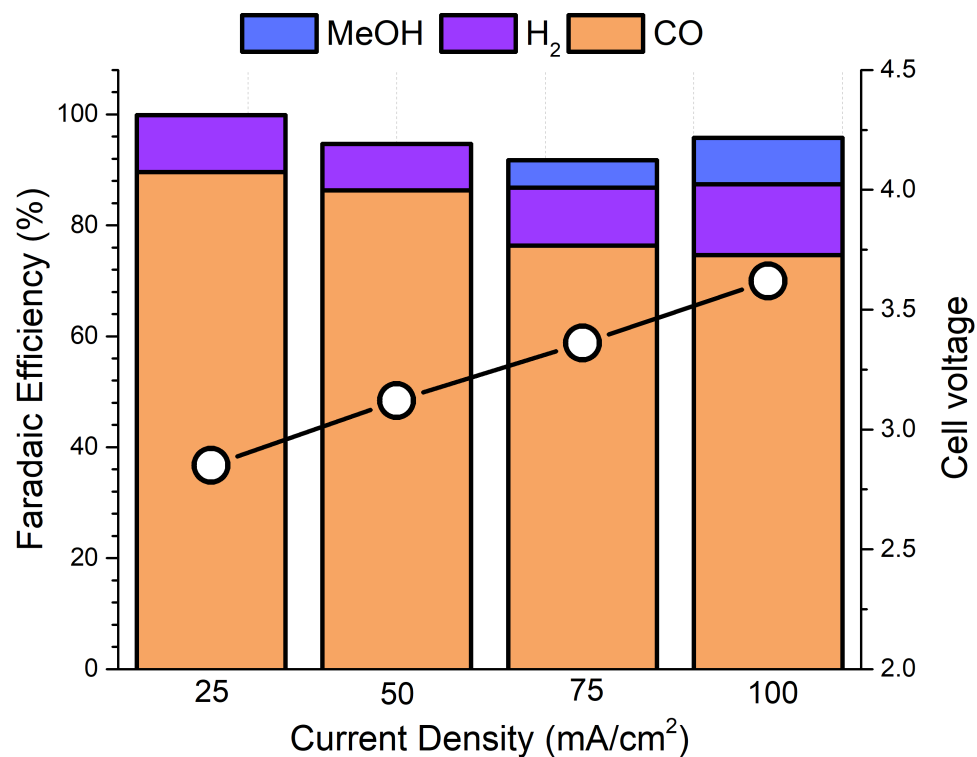


Xiaoping Wang  
(Myers)



# Progress and Outcomes: Task 3

At low current densities, CO formation with high FEs.  
As the current density increases, MeOH formation observed  
(~10% FE at 100 mA/cm<sup>2</sup>).

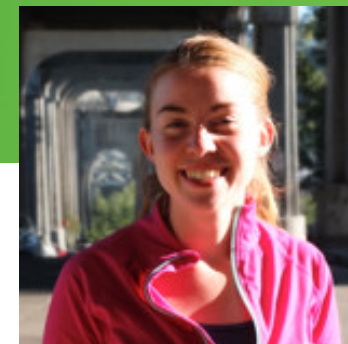


Danielle Henckel  
(Smith)

**CO<sub>2</sub> electrolyzer**  
**Cathode:** 1.1 mg/cm<sup>2</sup> CoPc/CNT/CF on GDE; **Anode:** Ni-foam  
**Membrane:** Fumasep BPM  
**Catholyte:** 0.4 M K<sub>2</sub>SO<sub>4</sub>  
**Anolyte:** 1 M KOH  
**Conditions:** 60 °C, 95% RH, 1 SPLM CO<sub>2</sub>

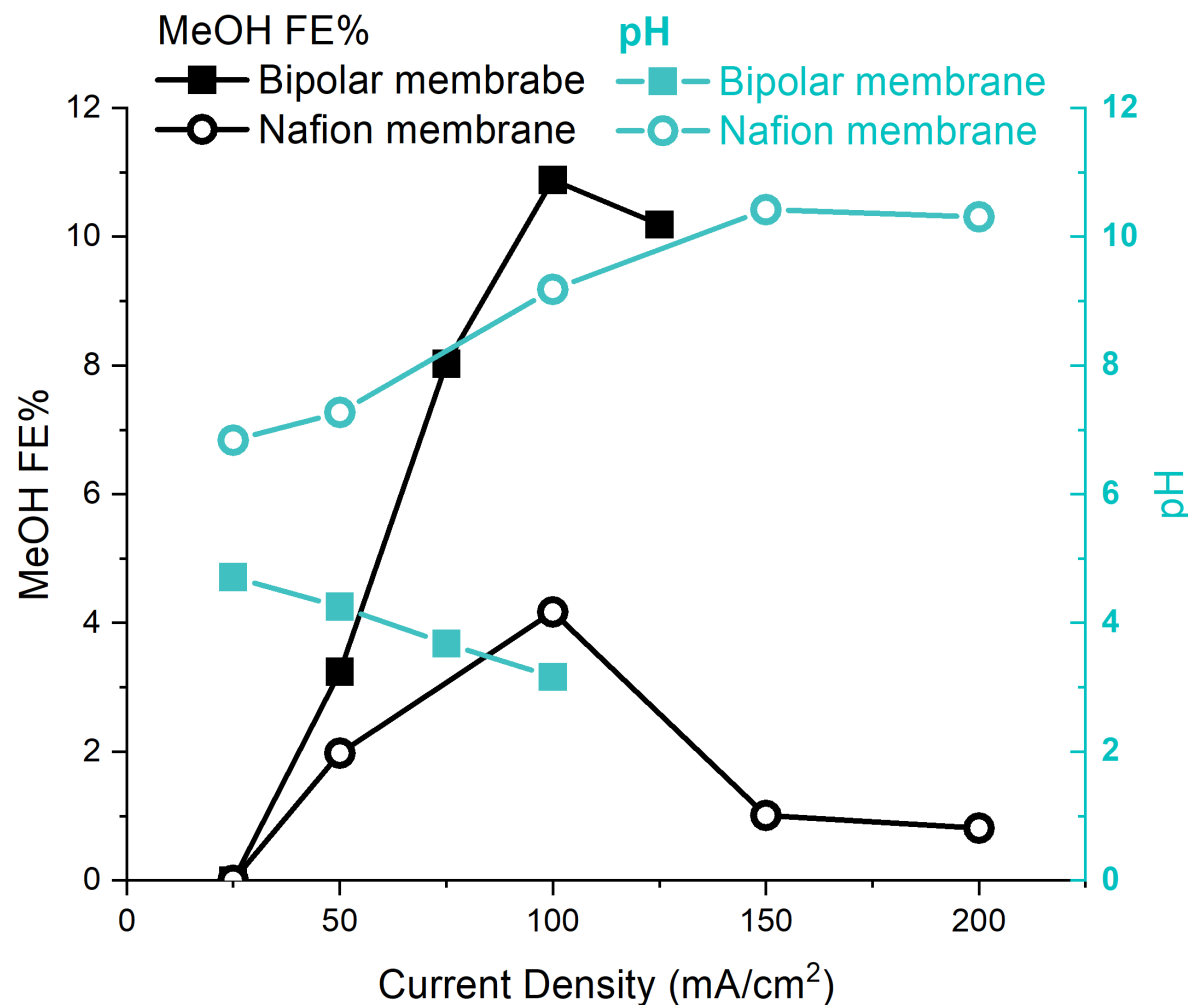


# Progress and Outcomes: Task 3



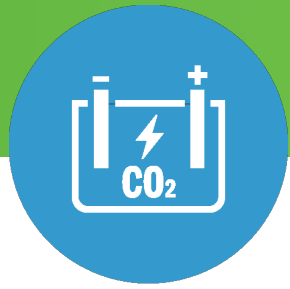
Danielle Henckel  
(Smith)

The pH of the electrolyte makes a big difference:



Lower the pH,  
higher the MeOH yield!





- Materials for  $\text{CO}_2$  to  $\text{CH}_3\text{OH}$  electrolyzers
- Co-macrocycle/carbon electrode hybrid catalysts
- 11%  $\text{CH}_3\text{OH}$  Faradaic efficiency achieved
- ~80% CO Faradaic efficiency achieved
- Collaboration with Ling Tao on TEA analysis

# Thank You

DOE – Kevin Craig  
**Ian Rowe**  
Robert Natelson

ANL - Michael Wang  
Amgad Elgowainy

LLNL - **Chris Hahn**

LBNL - Steve Singer  
Eric Sundstrom

NREL - **Michael G Resch**  
Ella Zhou  
Hariswaran Sitaraman  
Wei Xiong  
Jack Ferrell  
Gary Grim  
**Ling Tao**  
K.C. Neyerlin  
Chris Johnson  
Kimmy Mazza  
Amie Sluiter